

Pilot-Scale Silicone Process for Low-Cost CO₂ Capture

GE Global Research



**GE Global
Research**

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**2016 NETL CO₂ Capture
Technology Meeting
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Overview

Program Team

 **GE Global Research**

- Pilot-scale design
- Construction/Operation of Continuous System
- EH&S Assessment
- Techno-economic Assessment
- Plant Modeling


 **National Carbon Capture Center**


- Pilot-scale Operation
- Assessment of Data
- Integration of Components




36 Month, \$6.7MM Program to Advance the Amino-Silicone Solvent Process for CO₂ Capture to Pilot Scale

Program Objectives: Design and optimize a new process for a novel silicone CO₂ capture solvent and establish scalability and potential for commercialization of post-combustion capture of CO₂ from coal-fired power plants. A primary outcome will be a system capable of 90% capture efficiency with less than \$40/tonne CO₂ capture cost.

 **Design & Optimize Process**

 **Establish Scalability & Commercial Value**

 **Pilot of Post-Combustion CO₂ Capture**

Technical Approach

- Design and construct pilot-scale unit and obtain parametric data to determine key scale-up parameters
- Perform an EH&S and technical and economic assessment to determine feasibility of commercial scale operation
- Develop scale-up strategy

Outcomes

- Strategy for future scale-up
- Technical and economic feasibility determined
- Environmental assessment

Anticipated Benefits of the Proposed Technology

- 90% CO₂ Capture
- \$40/tonne CO₂ capture cost

• Continuation of previous DOE/NETL funded project (DE-FE0007502)

Scope

Phase I: 1/1/2014 - 12/31/2014

(\$1.5MM with 20% GE cost share)

- ✓ Develop preliminary process models and perform preliminary techno-economic analysis
- ✓ Perform preliminary EH&S risk assessment
- ✓ Design and construct pilot-scale aminosilicone desorber skid

Phase II: 1/1/2015 - 12/31/2016

(\$5.2MM with 20% GE cost share)

- ✓ Integrate skid with the NCCC pilot-scale system
- ✓ Water commissioning of pilot-scale system
- ✓ Study lower desorber residence times
 - ✓ Can decrease residence time by 60%
- ✓ Investigate corrosion inhibitors
 - ✓ Identified additive that decreases corrosion of carbon steel by 90%
- Develop solvent recovery methods

Scope Cont.: Items to be Completed

Phase II: 1/1/2015 - 12/31/2016

(\$5.2MM with 20% GE cost share)

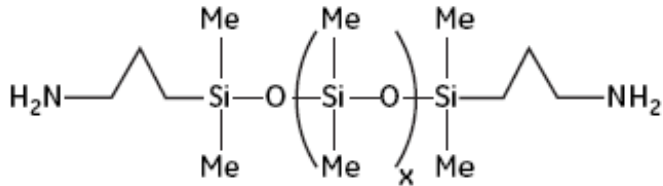
- ✓ Test steam stripper design at bench-scale
- Perform pilot-scale testing (starting August 2016)
 - Test both CSTR and steam stripper designs
- Analyze data from pilot tests at 0.5 MW scale
- Perform techno-economic analysis and update cost of carbon capture
- Perform technology EH&S risk assessment
- Develop cost estimate for full-scale manufacture of solvent

Summary of Solvent Advantages

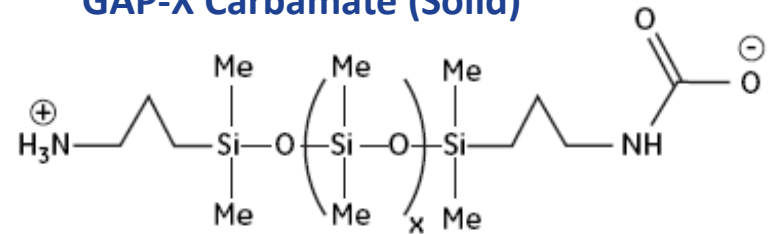
- Lower volatility
 - Simplified separations
 - Less energy wasted vaporizing solvent and/or water
 - Lower airborne release rates
- Lower heat capacity
- Reduced corrosion
- Possibly higher mass transfer rates
- Potentially decreased issues with aerosol formation

Absorbent

GAP-X (Liquid)



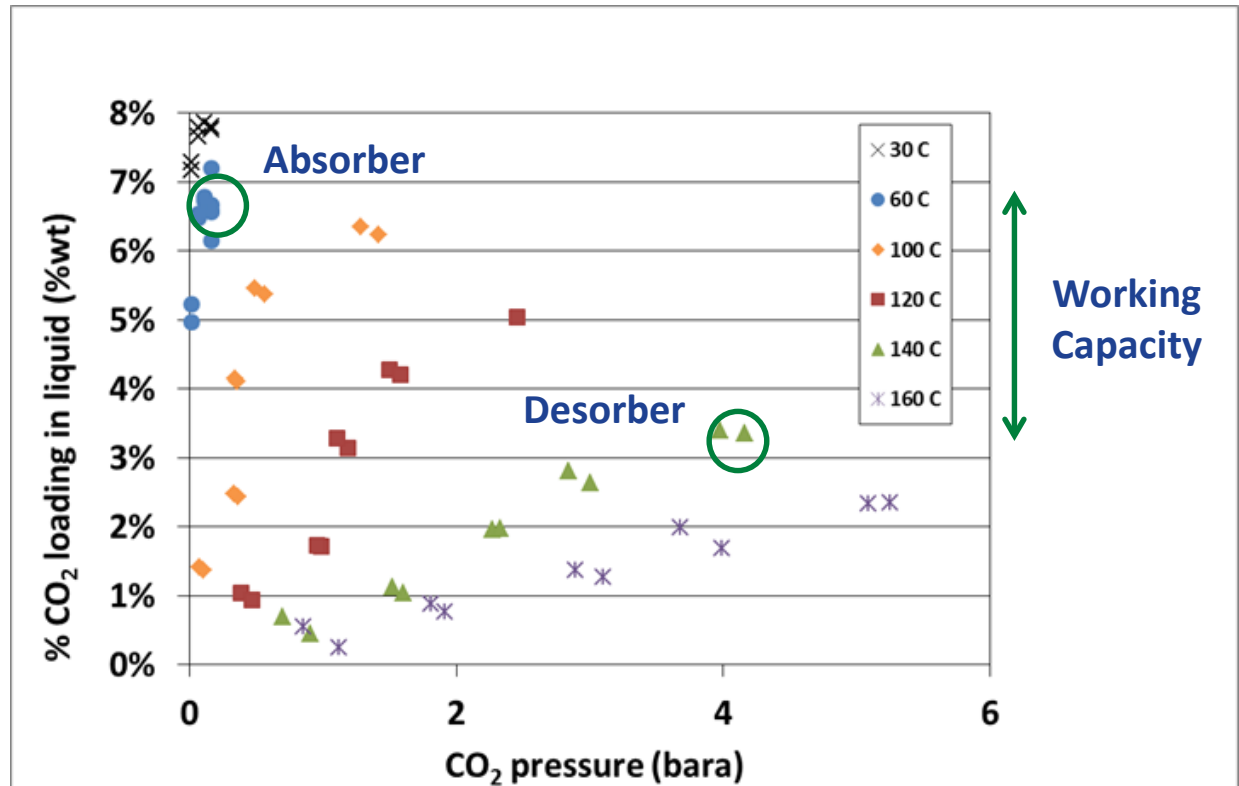
GAP-X Carbamate (Solid)



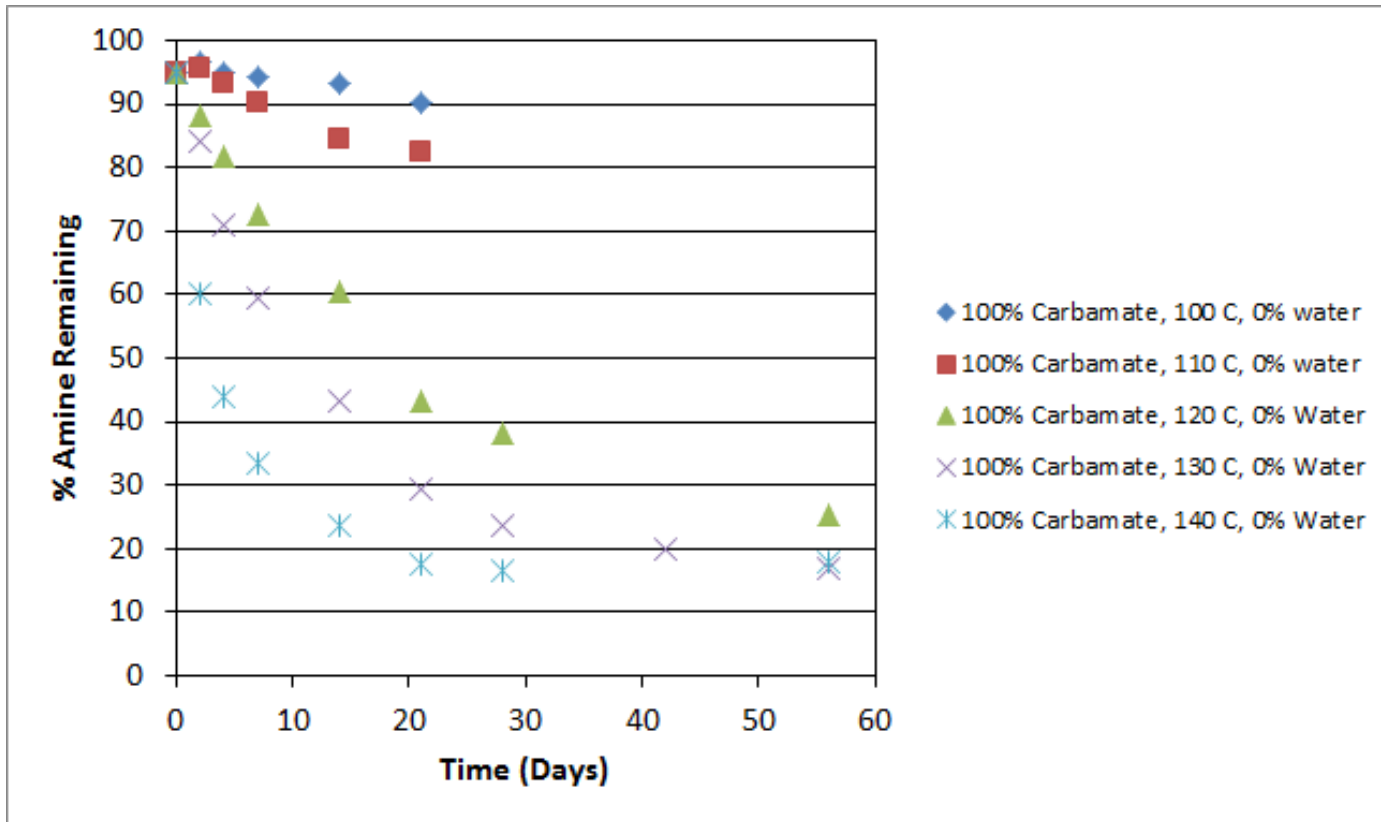
GAP-1_m Absorbent Composition

- 40% GAP-0
- 33% GAP-1
- 19% GAP-2
- 8% GAP-3

Carbamate does not precipitate in a GAP-1_m/TEG mixture

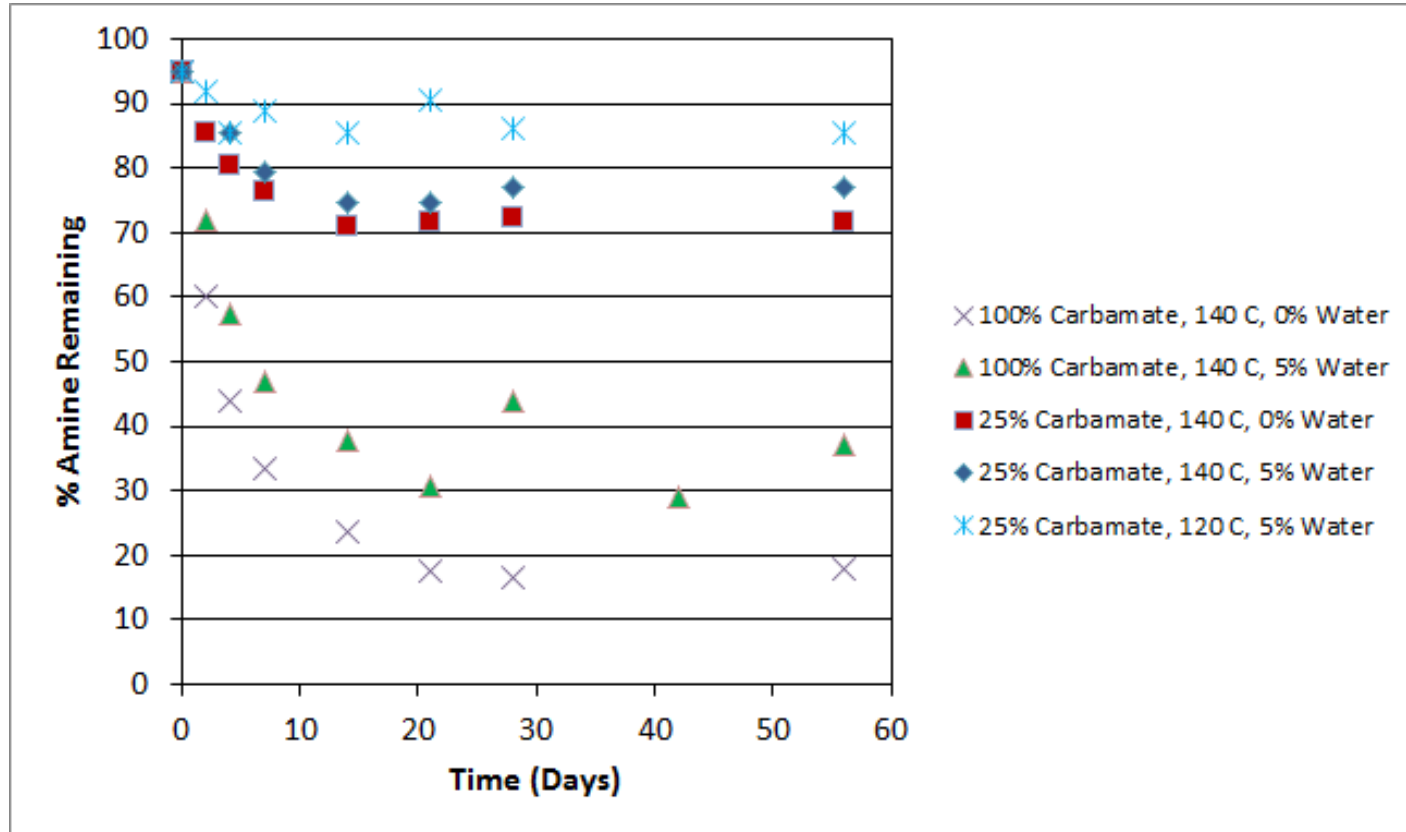


Accelerated Thermal Degradation Testing



- Tests conducted in pressure cells with continuous heating
- High thermal degradation at 100% CO₂ loading and 140 °C

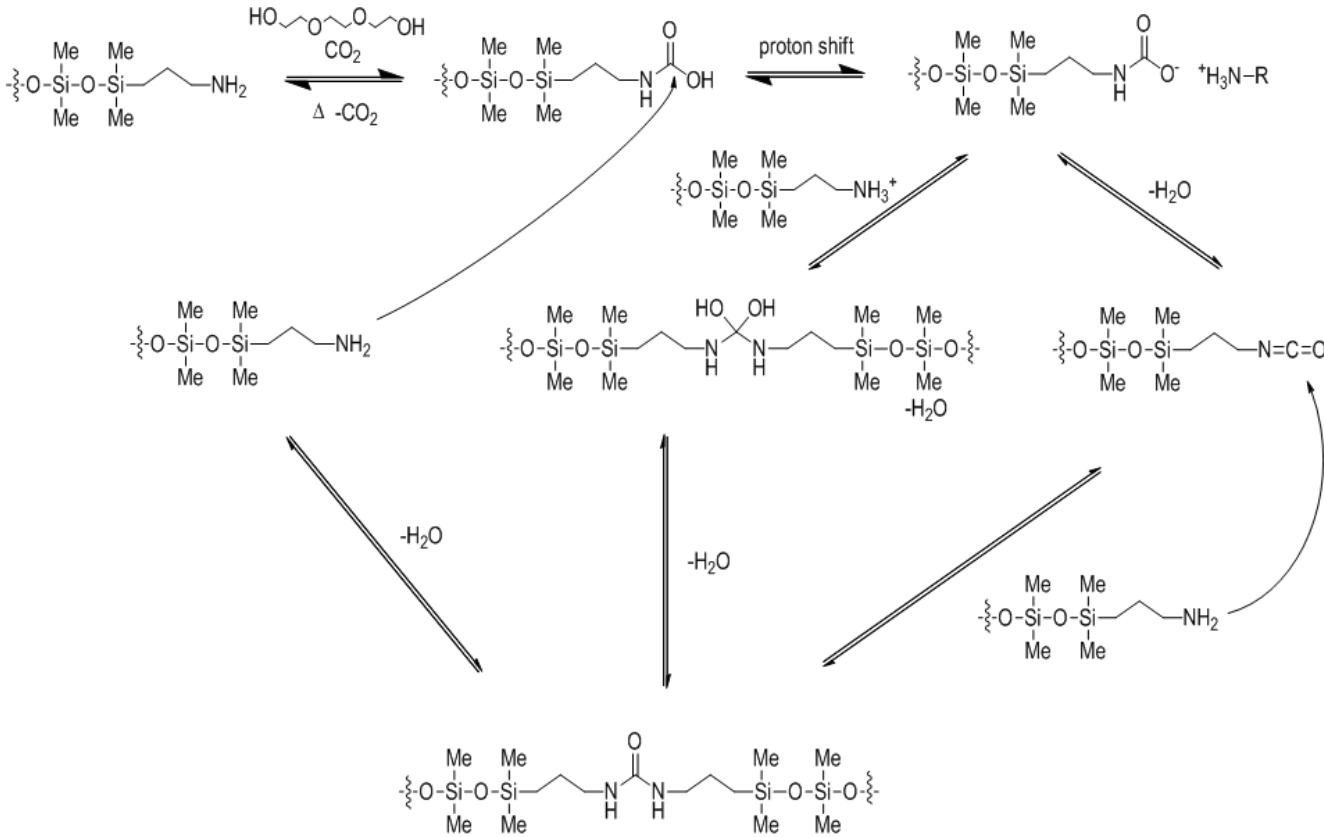
Thermal Degradation Mitigation



Ways to lower thermal degradation

- Lower temperature
- Lower carbamate loading
- Add water

Thermal Degradation Pathway

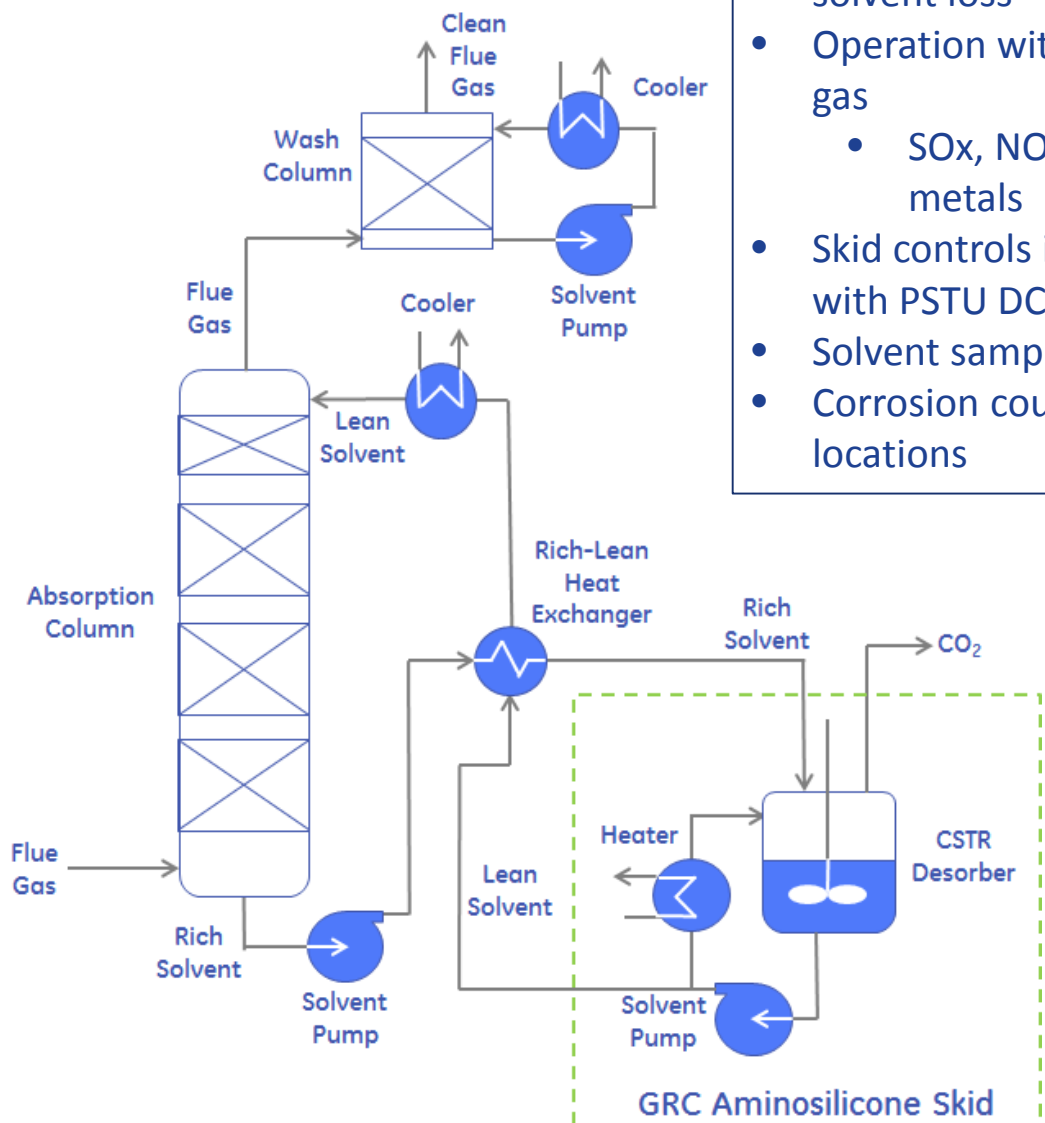


Urea Degradation Product

- Pathway demonstrates why water inhibits the thermal degradation of the solvent and high CO_2 loading facilitates degradation
- Currently working on methods for reversing formation of urea

Pilot-Scale Process

The NCCC PSTU



- Ability to measure solvent loss
- Operation with real flue gas
 - SO_x, NO_x, heavy metals
- Skid controls integrated with PSTU DCS
- Solvent sampling points
- Corrosion coupon testing locations

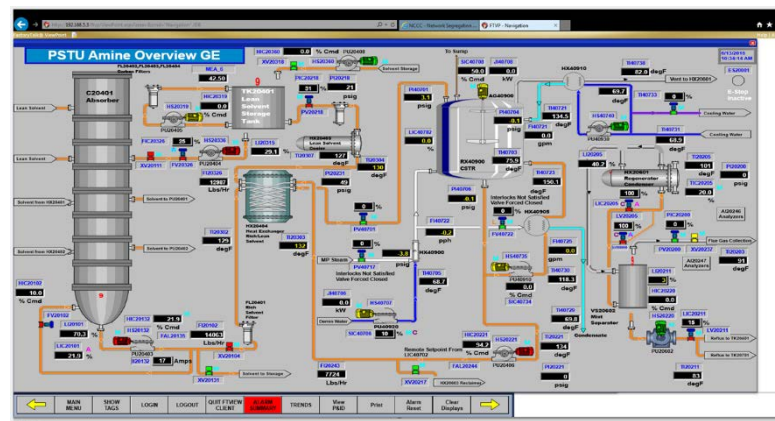
NCCC Pilot Started

- ✓ Integration of skid with PSTU
- ✓ Water commissioning, Dec. 2015

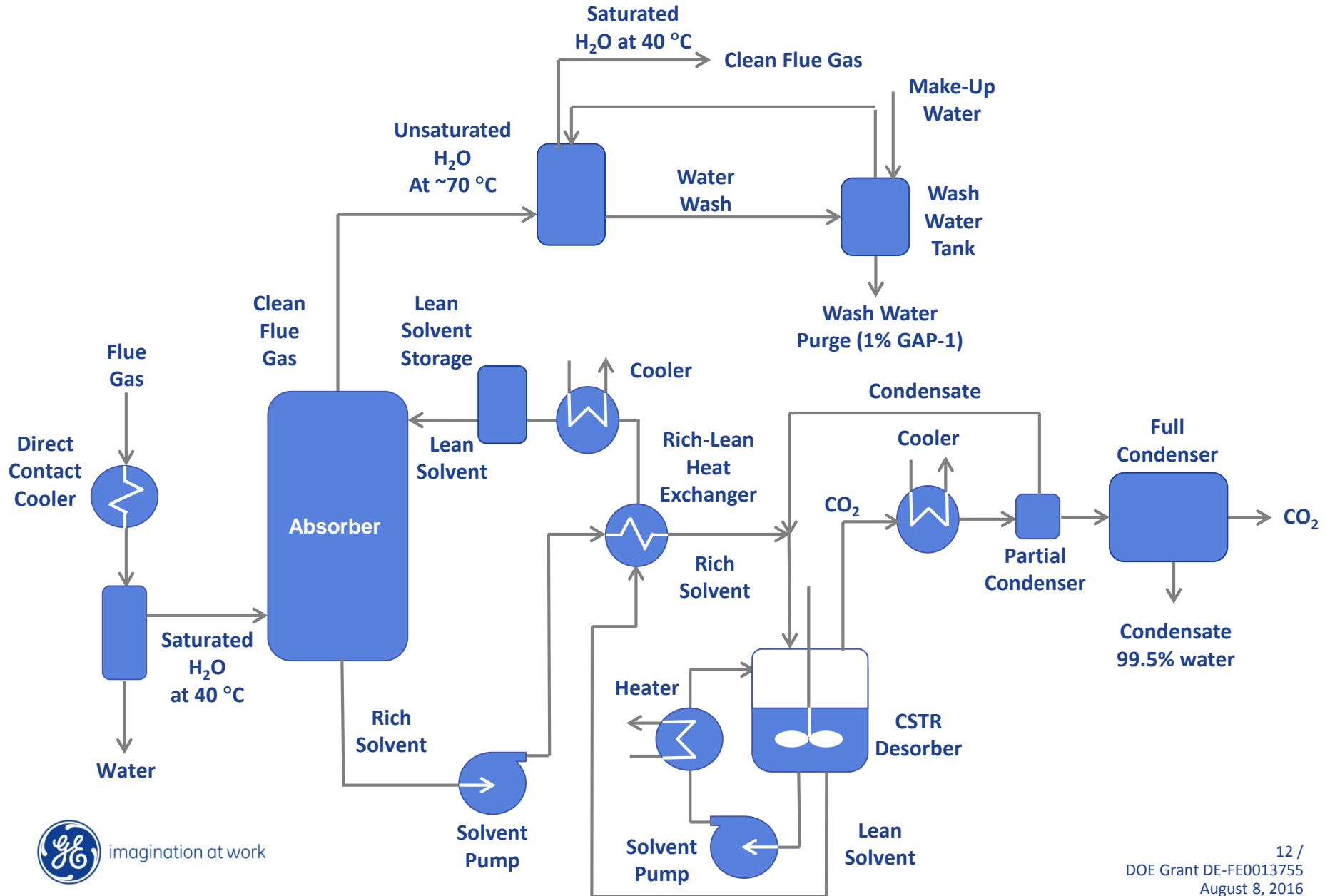
Pilot test

- ✓ Test matrix, sampling & analytical plan determined
- ✓ Mid-May: BOP startup, steam & flue gas available
- ✓ New bag house... reduce solvent loss from aerosol
- ✓ Steam commissioning completed with regenerator
- ✓ Steam commissioning with CSTR
- ✓ Solvent loaded
 - Test window: August through October... test both CSTR and steam stripper

Pilot-scale test skid



Original Process Concept



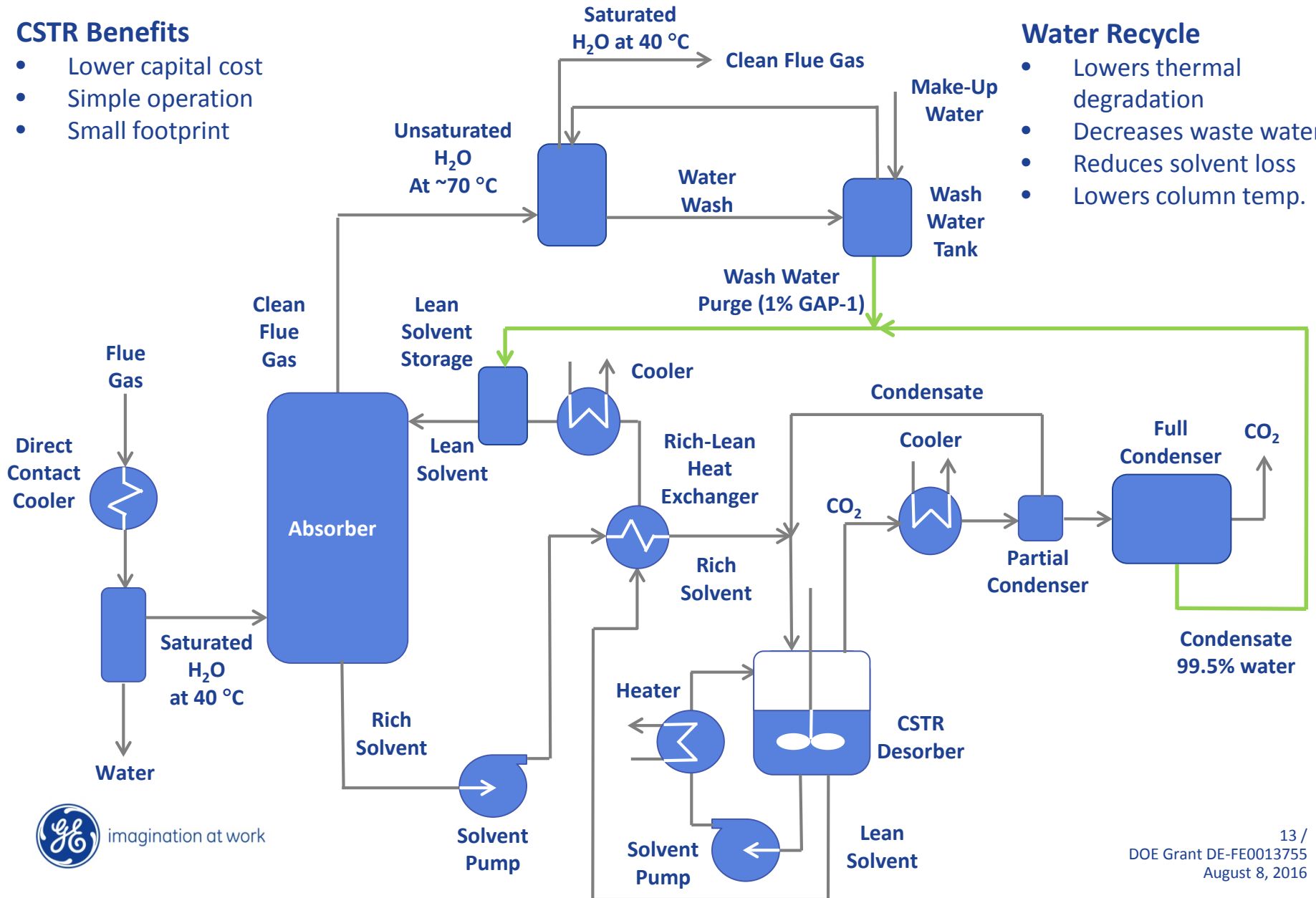
Process Design with CSTR and Water Recycle

CSTR Benefits

- Lower capital cost
- Simple operation
- Small footprint

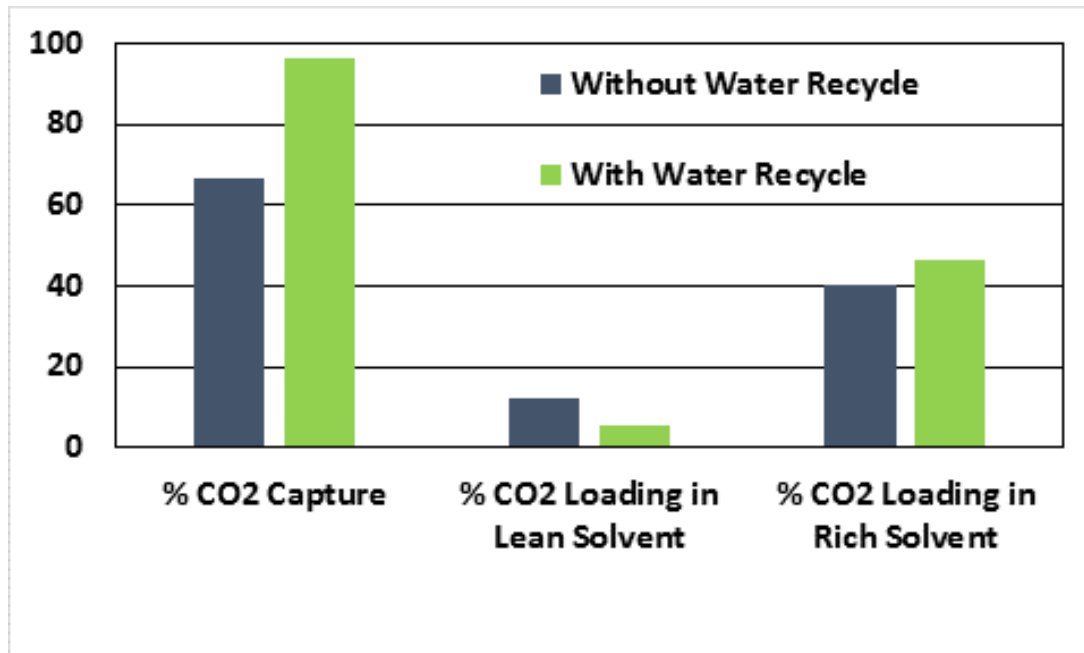
Water Recycle

- Lowers thermal degradation
- Decreases waste water
- Reduces solvent loss
- Lowers column temp.



Predicted Performance

- Process model evaluation of system performance



- **Process conditions**

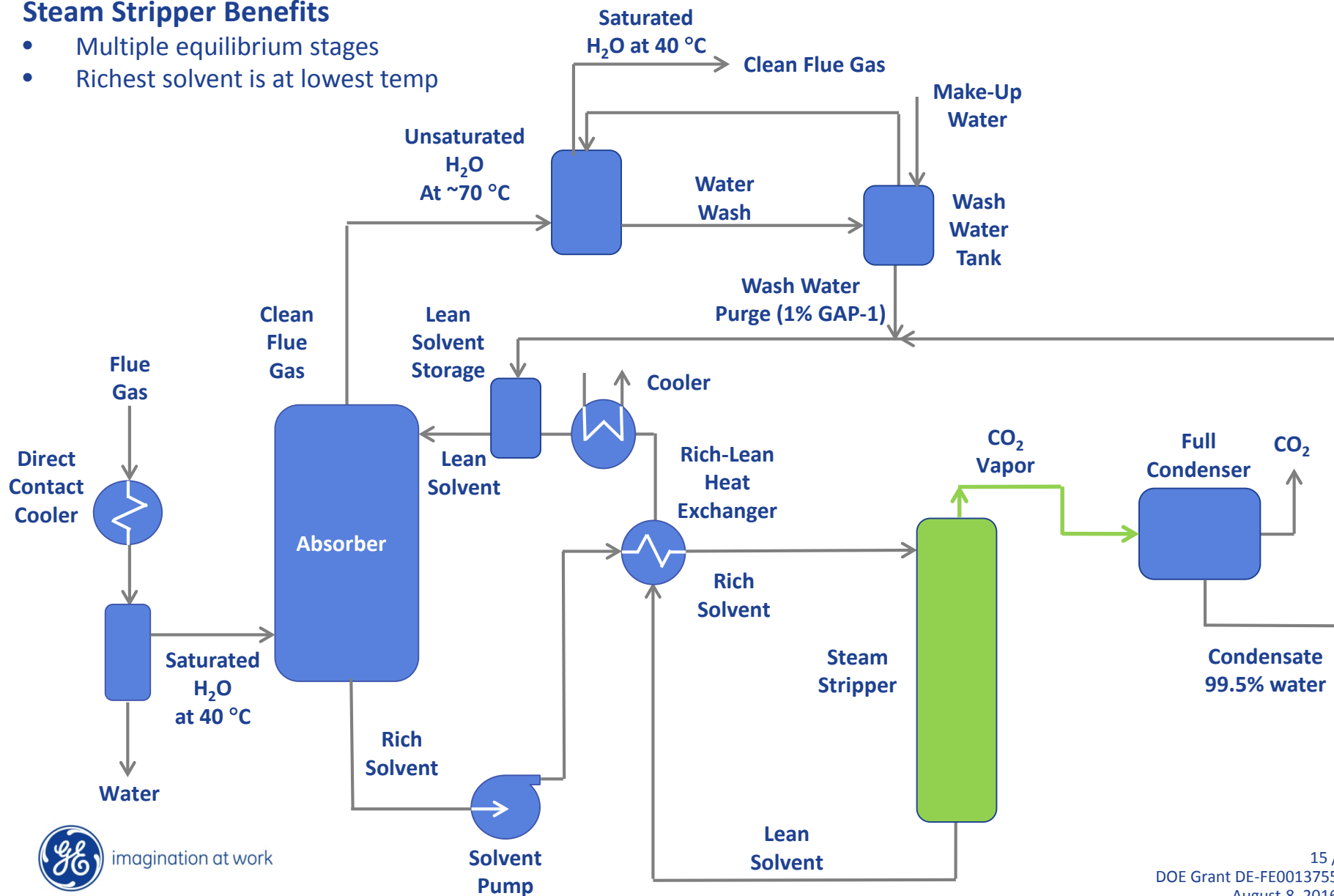
- Flue Gas CO₂ Concentration = 12.2%
- Flue Gas Inlet Temp. = 43.3 °C
- Flue Gas Flow Rate = 2270 kg/hr
- Desorber Pressure = 1 bara
- Cooling Water Temp. = 32 °C

- Water recycle enhances capture performance

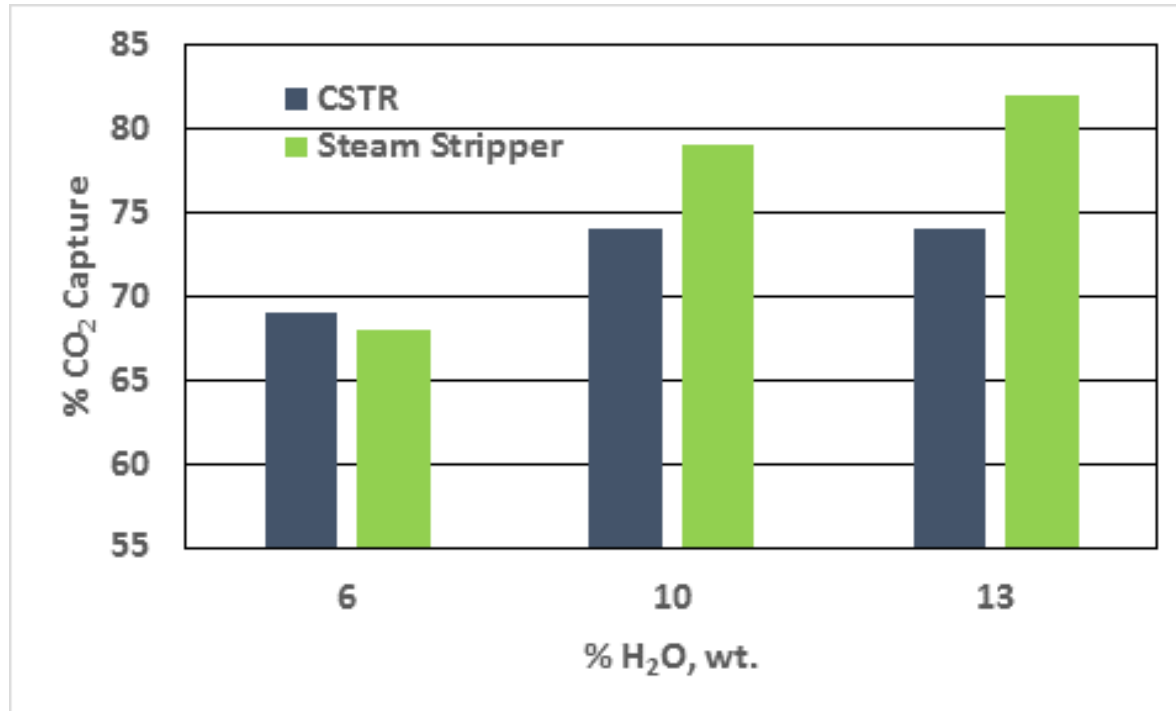
Process Design with Steam Stripper

Steam Stripper Benefits

- Multiple equilibrium stages
- Richest solvent is at lowest temp



Steam Stripping at Bench-Scale



Process conditions

- $T_{\text{reboiler}} = 108 \text{ }^{\circ}\text{C}$
- Flue Gas CO₂ Concentration = 12%
- Flue Gas O₂ Concentration = 5% O₂
- Flue Gas SO₂ Concentration = 1 ppm

Future Work

- 2016
 - Operate PSTU with CSTR desorber for 1.5 months (starting in August)
 - Operate PSTU with steam stripper for 1.5 months (starting in September)
 - Use data to update process models
 - Update Techno-Economic Analysis and EH&S Risk Assessment
- Beyond
 - Work with solvent manufacturers to lower solvent cost
 - NETL has funded GE to evaluate performing demo-scale (10 MW) test at TCM
 - Continue developing
 - Methods for reducing oxidative degradation
 - Solvent reclamation processes

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